

Figure captions

Figure 1: Schematic diagram of the laboratory-scale forward osmosis (FO) system.

Figure 2: Schematic diagram of the laboratory-scale (NF) nanofiltration system.

Figure 3: Zeta potential of the HTI and NF90 membranes as a function of pH. The background electrolyte solution was 1 mM KCl.

Figure 4: Water flux as a function of time at different draw solution (NaCl) concentrations in (a) PRO mode and (b) FO mode. Both feed and draw solution temperatures were 22.5 ± 1 °C and the cross-flow velocity at both sides of the membrane was 9 cm/s. Milli-Q water was used as the feed solution (pH 6).

Figure 5: Water and reverse salt flux at different draw solution (NaCl) concentrations in PRO and FO modes. Experimental conditions are as described in Figure 4.

Figure 6: The rejection of charged TrOCs by the HTI and NF90 membranes as a function of molecular weight at different draw solution (NaCl) concentrations in (a) PRO, (b) FO and (c) RO modes. Compounds not detectable in the permeate samples are denoted by *, #, and & corresponding to the PRO, FO, and RO modes, respectively. Experiments conducted in RO mode were in recirculation configuration, with a feed temperature of 22.5 ± 1 °C, cross-flow velocity of 30.4 cm/s, and permeate flux of approximately 14.6 L/m²h. Other experimental conditions are as described in Figure 4.

Figure 7: The rejection of neutral TrOCs by the HTI and NF90 membranes as a function of molecular weight at different draw solution (NaCl) concentrations in (a) PRO, (b) FO and (c) RO modes. Compounds not detectable in the permeate samples are denoted by *, #, and & corresponding to the PRO, FO, and RO modes respectively. Experimental conditions are as described in Figure 6.

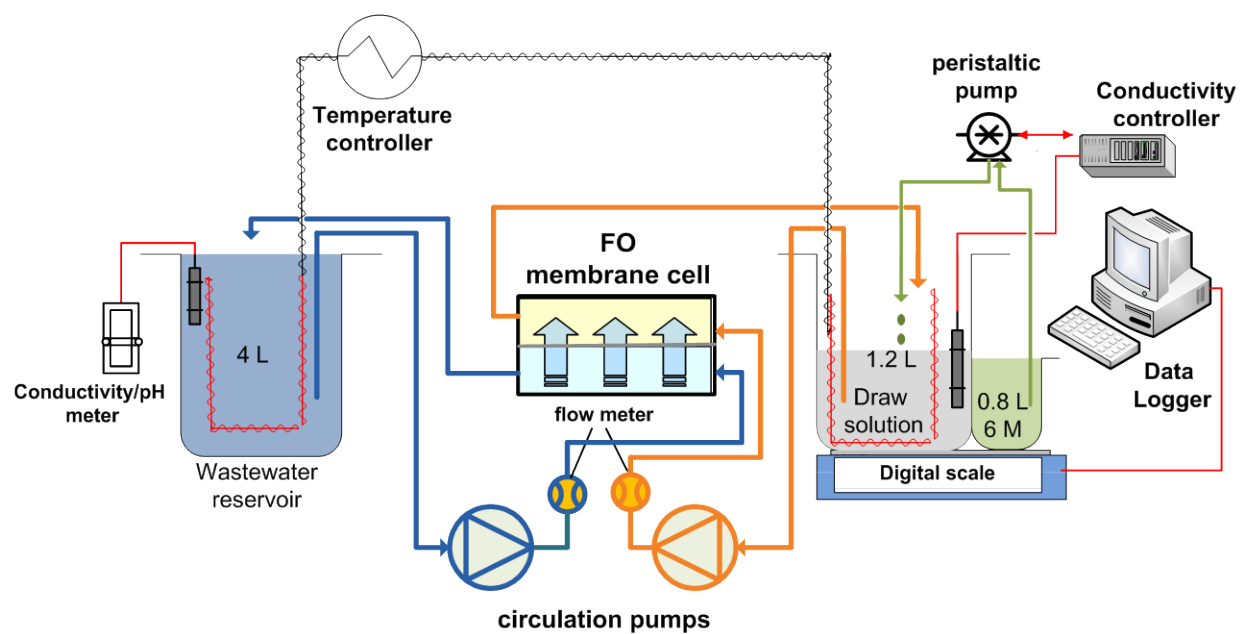


Figure 1

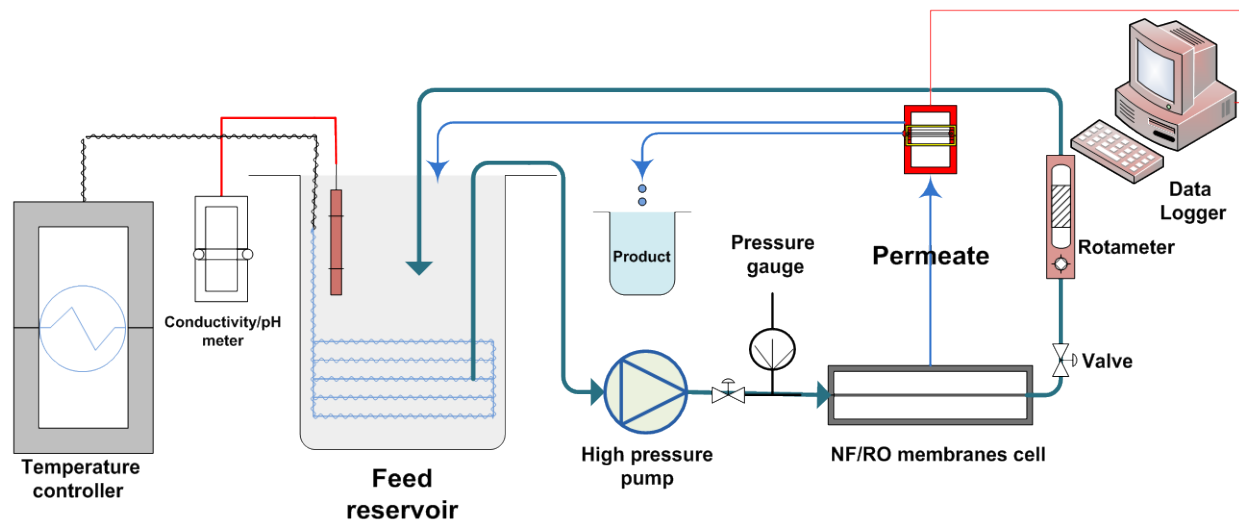


Figure 2

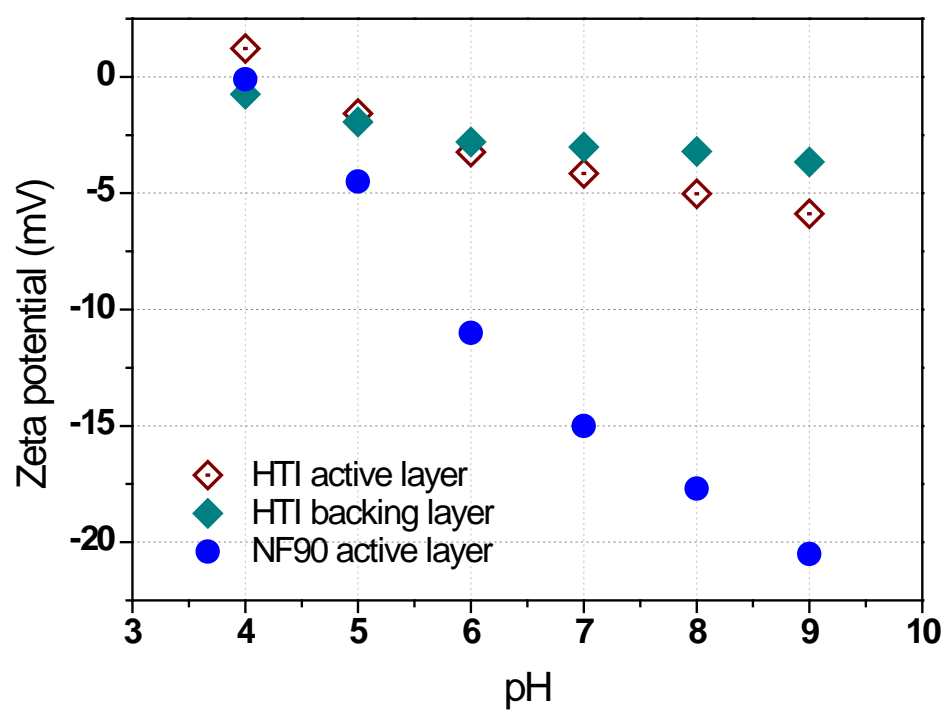


Figure 3

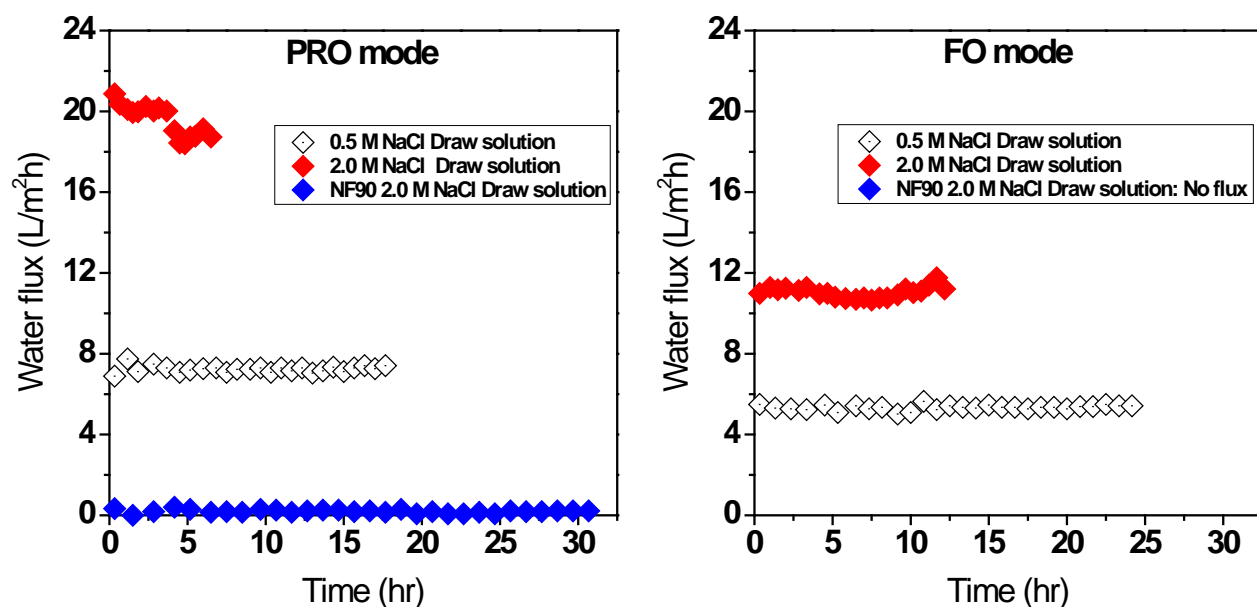


Figure 4

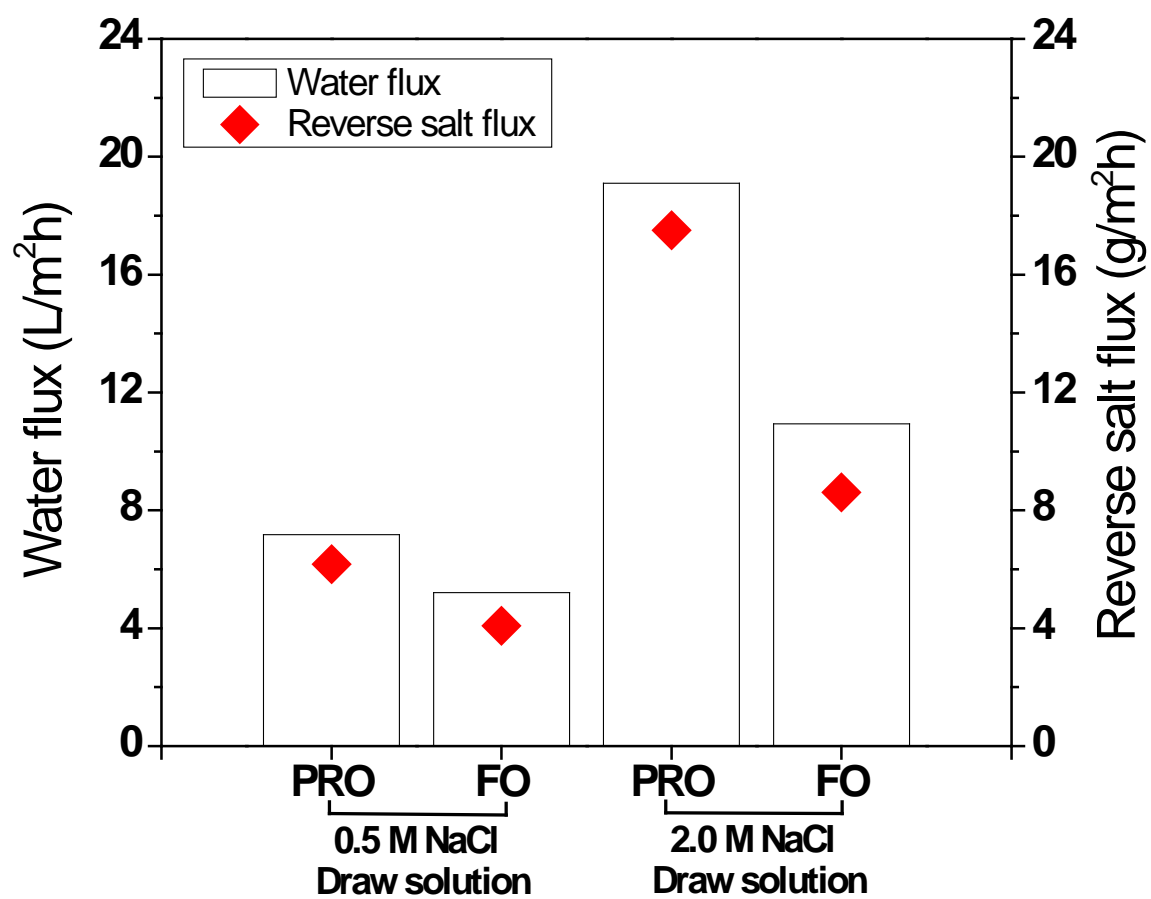


Figure 5

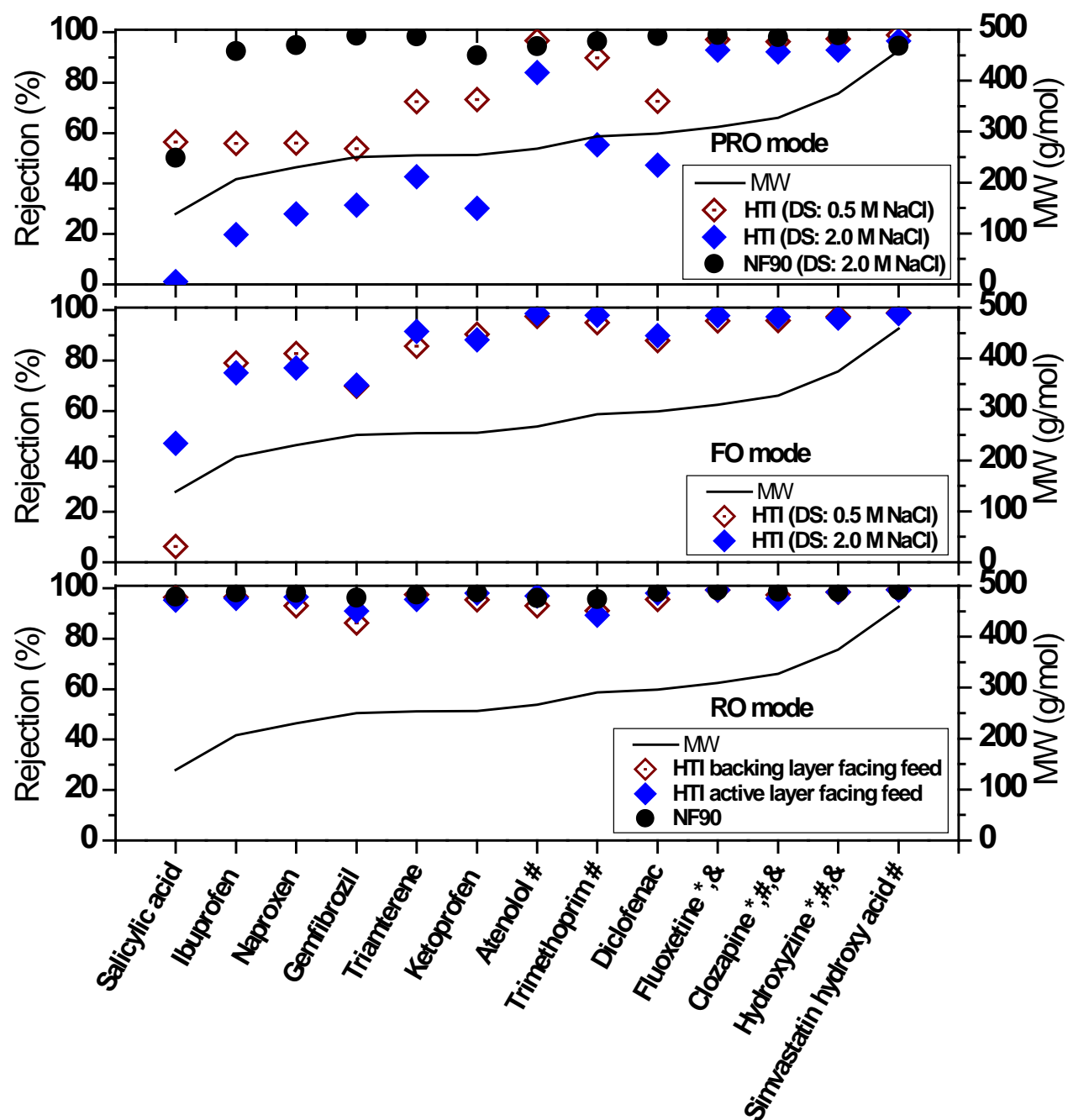


Figure 6

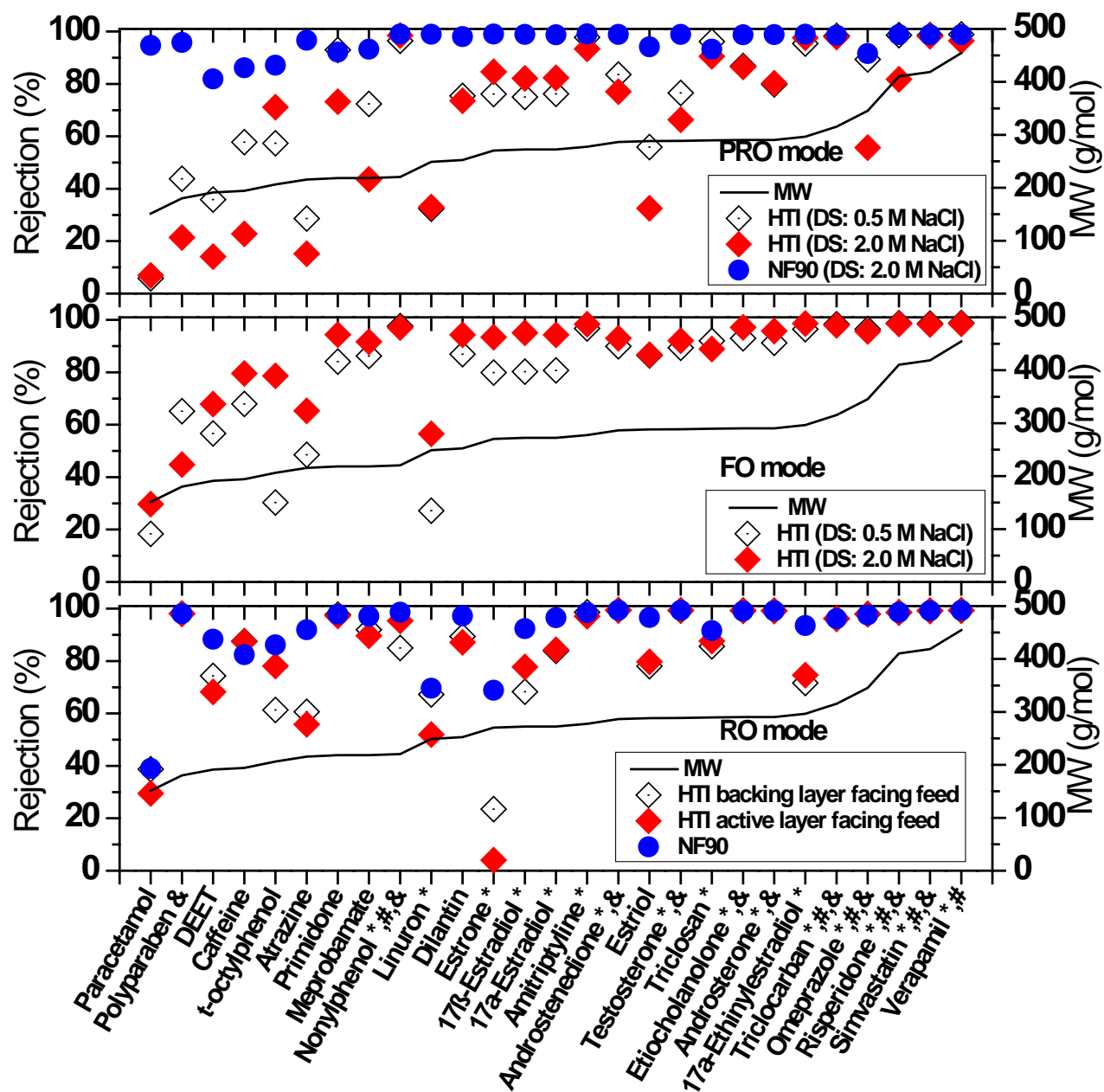


Figure 7